Chapter 1: Introduction to Transport Phenomena in Materials Processing

Chapter 2: Steady State Conduction Heat Transfer

p. 109: Problem 2.1(c):

- q"=10 W/m²K, not 100 W/m²K
- The Ar is effectively not moving, even though it is a fluid, because the thickness of the gap between the two panes is so small.
- In part (c), where it says "thickness of the air gap", it should read "thickness of the Ar gap".

p. 112: Problem 2.11: Use T_{sink}=40°C.

p. 113: Problem 2.13: The height and width of the aluminum are H and W, while the thickness of the trough wall is t.

p. 115: Problem 2.15: Use (c) graphite (*k* = 1.9 W/mK) and (e) magnesia (*k* = 0.085 W/mK).

p. 115: Problem 2.18: The convection occurs at $x = -L_p$ rather than $x = L_p$.

Chapter 3: Transient Conduction Heat Transfer

p. 139: The equation at the bottom of the page should read

$$\lim_{x\to\infty}\theta(\varepsilon=1,\tau)=\exp(-\infty)\left[1^2-2(1)\right]+1=1$$

p. 139: Eqtn. (3.42) should read

$$\theta = \exp\left(-3\tau\right)\left[\varepsilon^2 - 2\varepsilon\right] + 1$$

p. 177, Problem 3.8: Part (b) should end with "(*t* < *t*_{crit})", not "(*t* =0)."

p. 178, problem 3.10: The phrase "...on the Figure 3.28." should be removed.

p. 179, problem 3.13: The first sentence should read: "The temperature of an effectively semiinfinite slab of steel, initially at uniform temperature ($T_i = 25$ °C) is raised instantaneously to 50 °C at the wall."

p. 182, problem 3.25: Use $M_f = 0.1 \text{ m}$ and $T_o = 70^{\circ}\text{C}$.

p. 182, problem 3.26: Use $L_f = 2.98 \times 10^5 \text{ J/kg}$.

<u>Chapter 4: Mass Diffusion in the Solid State</u> **p. 205**: The right hand side of eqtn (4.45) should read

$$= \left(\frac{C_{Ai}^2 - C_A^{2^*}}{C_A^{1^*} - C_A^{2^*}}\right) \sqrt{\frac{D_A^2}{3t}}$$

p. 205: The quadratic equation between (4.46) and (4.47) should read

$$\phi^2 - \frac{1}{\sqrt{3}} \left[\frac{C_{Ai}^2 - C_A^{2*}}{C_A^{1*} - C_A^{2*}} \right] \phi + \frac{1}{2} \frac{D_A^1}{D_A^2} \left[\frac{C_A^{1*} - C_{Ao}^1}{C_A^{1*} - C_A^{2*}} \right] = 0$$

p. 205: Equation (4.47) should read

$$\phi = \frac{1}{2\sqrt{3}} \left[\frac{C_{Ai}^2 - C_A^{2^*}}{C_A^{1^*} - C_A^{2^*}} \right] \left[1 + \sqrt{1 - 6\left(\frac{D_A^1}{D_A^2}\right) \left(\frac{C_A^{1^*} - C_A^{2^*}}{C_{Ai}^2 - C_A^{2^*}}\right) \left(\frac{C_A^{1^*} - C_{Ao}^1}{C_{Ai}^2 - C_A^{2^*}}\right)} \right]$$

p. 228, problem 4.6: Part (c) should read: "(c) Write the expression for solute flux continuity at the interface. Scale this relationship using these reference values, $\Delta C^A = C_o^A - C_{Int}$ and $\Delta C^B = C_{Int} - C_o^B$, and the result from part (b). Find an estimate for the interface composition, C_{Int} , in terms of properties and the initial compositions."

p. 231, problem 4.10: Part (c) should read
$$D_{Al}^{\alpha} \approx 3.9 \times 10^{-5} \left(\frac{\text{m}^2}{\text{s}}\right) \exp\left(-\frac{155,000 \text{ J/mole}}{RT}\right)$$

Chapter 5: Hydrostatics

p. 249, problem 5.10: The figure 5.15 should read:



<u>Chapter 6: Mechanical Energy Balance in Fluid Flow</u> **p. 278,** problem 6.2: Assume a smooth pipe (no roughness).

p.281, problem 6.10: The frictional loss should be 120 J/kg, not 120 J/km. Use ρ = 870 kg/m³ and μ =0.8 kg/ms

<u>Chapter 7: Equations of Fluid Motion</u> **p. 287**: The second part of the equation between Eq. (7.7) and Eq. (7.8) should read

$$\dot{m}_{y+dy} = \rho \, v_{y+dy} A_{y+dy}$$

p. 303, problem 7.2: Use δ = 0.01 m.

p. 304, problem 7.3: The second sentence should read "Motion in the fluid is started by a sudden change in fluid velocity from zero to a characteristic value, *U*_o, uniform in the *x* direction."

Chapter 8: Internal Flow

p. 320, Figure 8.8: label of gravitational force in figure should read

$$\overline{g} = g_z \hat{z} = -g \hat{z}$$

p. 354, problem 8.1: "*r* = 1000 rpm" should be "ω = 1000 rpm".

p. 355, problem 8.8: The last section should read "Solve the system for the velocity field and sketch w(r)." A sketch of u(r) would be a horizontal line at u = 0!

p. 355, problem 8.9: This problem should refer to Figure 8.23, not Figure 8.24.

Chapter 9: External Flows

p. 401, problem 9.12: $u_{ref} \ll \Omega R = v_{ref}$ should be added to the list of assumptions in problem statement. Also, The density of the photoresist is 1200 kg/m³.

<u>Chapter 10: Convection Heat Transfer</u> **p. 441**, Equation 10.77: Should be $\overline{Nu} = C \operatorname{Re}_{D}^{m} \operatorname{Pr}^{1/3}$

p. 466, Equation (10.148): Should be
$$\overline{Nu}_H = 0.68 + \left[\frac{0.67}{\left(\Pr^{9/16} + 0.671\right)^{4/9}}\right] \left(Ra_H \Pr\right)^{1/4}$$

p. 472, Eq. 10.160: Should have $\left(C_{sf}
ight)^{\!\!-\!\!3}$, not $\left(C_{sf}
ight)^{\!\!3}$.

p. 475, problem 10.2: Use D = 0.01 m.

p. 478-479, problem 10.13: Use q = 0.004 W = 4 mW

p. 480, problem 10.19: All the temperatures should be in Kelvin.

p. 480, problems 10.20 and 10.21: Use
$$h_{fg} = 2.3 \times 10^6 \frac{\text{J}}{\text{kg}}$$
 and $\sigma = 0.060 \text{ N/m}$.

Chapter 11: Mass Transfer in Fluids **p. 521,** problem 11.3: Le = 1

<u>Chapter 12: Radiation Heat Transfer</u> **p. 571**, problem 12.15: Use Figure 12.27 for this problem.

p. 572, problem 12.17:

- T_H = 600 K
- "Panel" should be replaced with "plate."
- The variable " w_s " should be replaced with " w_H ."

p. 573, problem 12.19: The tabulated view factor, F_{21} , is $F_{21} = \frac{1}{2} \left\{ 1 - \left[1 + \left(\frac{D}{L} \right)^2 \right]^{-1/2} \right\}$

Appendix II: Equations of motion and thermal energy balance

p. 579: The next to last terms in the three Navier-Stokes equations in Cartesian coordinates

should be $\frac{\partial}{\partial y} \left(\frac{\partial u}{\partial y} \right)$, $\frac{\partial}{\partial y} \left(\frac{\partial v}{\partial y} \right)$, and $\frac{\partial}{\partial y} \left(\frac{\partial w}{\partial y} \right)$.