

## Chapter 1: Introduction to Transport Phenomena in Materials Processing

### Chapter 2: Steady State Conduction Heat Transfer

**p. 109:** Problem 2.1(c):

- $q'' = 10 \text{ W/m}^2\text{K}$ , not  $100 \text{ W/m}^2\text{K}$
- The Ar is effectively not moving, even though it is a fluid, because the thickness of the gap between the two panes is so small.
- In part (c), where it says "thickness of the air gap", it should read "thickness of the Ar gap".

**p. 110:** Problem 2.3: The last line in the problem description should read "and the outer and inner heat transfer coefficients are, respectively,  $h_o = 75$  and  $h_i = 225 \text{ W/m}^2\text{K}$ ."

**p. 112:** Problem 2.11: Use  $T_{\text{sink}} = 40^\circ\text{C}$ .

**p. 113:** Problem 2.13: The height and width of the aluminum are H and W, while the thickness of the trough wall is t.

**p. 115:** Problem 2.15: Use **(c)** graphite ( $k = 1.9 \text{ W/mK}$ ) and **(e)** magnesia ( $k = 0.085 \text{ W/mK}$ ).

### Chapter 3: Transient Conduction Heat Transfer

**p. 139:** The equation at the bottom of the page should read

$$\lim_{x \rightarrow \infty} \theta(\varepsilon = 1, \tau) = \exp(-\infty) [1^2 - 2(1)] + 1 = 1$$

**p. 139:** Eqtn. (3.42) should read

$$\theta = \exp(-3\tau) [\varepsilon^2 - 2\varepsilon] + 1$$

**p. 172:** Eqtn. (3.129) should read

$$C_o = \left[ \frac{2(k\rho c)_m (T_M - T_i)}{3k_s \rho_s L_f} \right]^{1/2}$$

**p. 177,** Problem 3.8: Part (b) should end with " $(t < t_{\text{crit}})$ ", not " $(t = 0)$ ."

**p. 178,** problem 3.10: The phrase "...on the Figure 3.28." should be removed.

**p. 179,** problem 3.13: The first sentence should read: "The temperature of an effectively semi-infinite slab of steel, initially at uniform temperature ( $T_i = 25^\circ\text{C}$ ) is raised instantaneously to  $50^\circ\text{C}$  at the wall."

**p. 181,** problem 3.23: Assume  $T_i = 35^\circ\text{C}$ .

**p. 181,** problem 3.24:  $\alpha_m = 2.7 \times 10^{-7} \text{ m}^2/\text{s}$ .

**p. 182,** problem 3.25: Use  $M_f = 0.1 \text{ m}$  and  $T_o = 70^\circ\text{C}$ .

**p. 182**, problem 3.26: Use  $L_f = 2.98 \times 10^5 \text{ J/kg}$ .

**p. 183**, problem 3.28(c): The latent heat release rate should be  $\left[ \rho_L L_f A \frac{dM}{dt} \right]_{r=M}$ .

#### Chapter 4: Mass Diffusion in the Solid State

**p. 205**: The right hand side of eqtn (4.45) should read

$$= \left( \frac{C_{Ai}^2 - C_A^{2*}}{C_A^{1*} - C_A^{2*}} \right) \sqrt{\frac{D_A^2}{3t}}$$

**p. 205**: The quadratic equation between (4.46) and (4.47) should read

$$\phi^2 - \frac{1}{\sqrt{3}} \left[ \frac{C_{Ai}^2 - C_A^{2*}}{C_A^{1*} - C_A^{2*}} \right] \phi + \frac{1}{2} \frac{D_A^1}{D_A^2} \left[ \frac{C_A^{1*} - C_{Ao}^1}{C_A^{1*} - C_A^{2*}} \right] = 0$$

**p. 205**: Equation (4.47) should read

$$\phi = \frac{1}{2\sqrt{3}} \left[ \frac{C_{Ai}^2 - C_A^{2*}}{C_A^{2*} - C_A^{1*}} \right] \left[ 1 + \sqrt{1 - 6 \left( \frac{D_A^1}{D_A^2} \right) \left( \frac{C_A^{1*} - C_A^{2*}}{C_A^{2*} - C_A^{1*}} \right) \left( \frac{C_A^{1*} - C_{Ao}^1}{C_A^{2*} - C_A^{1*}} \right)} \right]$$

**p. 228**, problem 4.5: The diffusion coefficient for austenite should read

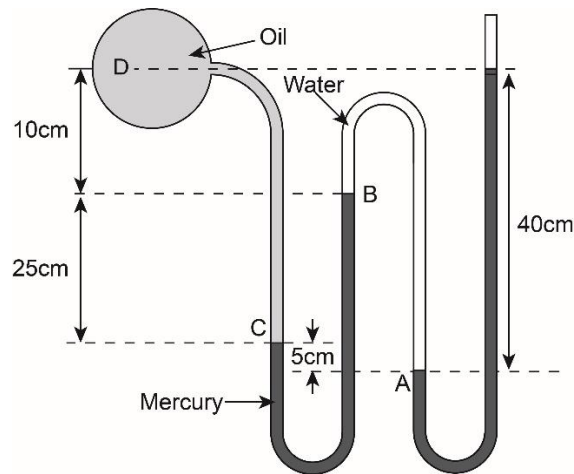
$$D_C^\gamma = 7 \times 10^{-6} \left( \text{m}^2/\text{s} \right) \exp \left[ - (133,900 \text{ J/gmol}) / RT \right]$$

**p. 228**, problem 4.6: Part (c) should read: “**(c)** Write the expression for solute flux continuity at the interface. Scale this relationship using these reference values,  $\Delta C^A = C_o^A - C_{Int}$  and  $\Delta C^B = C_{Int} - C_o^B$ , and the result from part (b). Find an estimate for the interface composition,  $C_{Int}$ , in terms of properties and the initial compositions.”

**p. 231**, problem 4.10: Part (c) should read  $D_{Al}^\alpha \approx 3.9 \times 10^{-5} \left( \frac{\text{m}^2}{\text{s}} \right) \exp \left( - \frac{155,000 \text{ J/mole}}{RT} \right)$

#### Chapter 5: Hydrostatics

**p. 249**, problem 5.10: The figure 5.15 should read:



### Chapter 6: Mechanical Energy Balance in Fluid Flow

**p. 278**, problem 6.2: Assume a smooth pipe (no roughness).

**p. 279**, problem 6.4: The mass flow rate should be  $\dot{m} = 7500 \text{ kg/s}$ .

**p. 281**, problem 6.8: The maximum allowable depth of the moving Al layer is  $h = 0.1 \text{ m}$  and the relative roughness is 0.0001.

**p. 281**, problem 6.10: The frictional loss should be  $120 \text{ J/kg}$ , not  $120 \text{ J/km}$ . Use  $\rho = 870 \text{ kg/m}^3$  and  $\mu = 0.8 \text{ kg/ms}$

### Chapter 7: Equations of Fluid Motion

**p. 287**: The second part of the equation between Eq. (7.7) and Eq. (7.8) should read

$$\dot{m}_{y+dy} = \rho v_{y+dy} A_{y+dy}$$

**p. 303**, problem 7.2: Use  $\delta = 0.01 \text{ m}$ .

**p. 304**, problem 7.3: The second sentence should read "Motion in the fluid is started by a sudden change in fluid velocity from zero to a characteristic value,  $U_o$ , uniform in the x direction."

### Chapter 8: Internal Flow

**p. 320**, Figure 8.8: label of gravitational force in figure should read

$$\bar{g} = g_z \hat{z} = -g \hat{z}$$

**p. 354**, problem 8.1: " $r = 1000 \text{ rpm}$ " should be " $\omega = 1000 \text{ rpm}$ ".

**p. 355**, problem 8.8: The last section should read "Solve the system for the velocity field and sketch  $w(r)$ ." A sketch of  $u(r)$  would be a horizontal line at  $u = 0$ !

**p. 355**, problem 8.9: This problem should refer to Figure 8.23, not Figure 8.24.

#### Chapter 9: External Flows

**p. 401**, problem 9.12:  $u_{ref} \ll \Omega R = v_{ref}$  should be added to the list of assumptions in problem statement. Also, The density of the photoresist is  $1200 \text{ kg/m}^3$ .

#### Chapter 10: Convection Heat Transfer

**p. 441**, Equation 10.77: Should be  $\overline{Nu} = C Re_D^m Pr^{1/3}$

**p. 458**: Re range on Eq. (10.124) should be  $2500 < Re_D < 10^7$ .

**p.464**: The term  $\left(\frac{\alpha x}{\delta_T^2}\right)$  in Eq. (10.142) should be  $\left(\frac{\alpha x}{\delta_T^2}\right)^2$ .

**p.465**: The term  $\left(\frac{x}{\delta}\right)$  in Eq. (10.144) should be  $\left(\frac{x}{\delta}\right)^2$ .

**p. 466**, Equation (10.148): Should be  $\overline{Nu}_H = 0.68 + \left[ \frac{0.67}{(Pr^{9/16} + 0.671)^{4/9}} \right] (Ra_H Pr)^{1/4}$

**p. 472**, Eq. 10.160: Should have  $(C_{sf})^{-3}$ , not  $(C_{sf})^3$ .

**p. 475**, problem 10.2: Use  $D = 0.01 \text{ m}$ .

**p. 478-479**, problem 10.13: Use  $q = 0.004 \text{ W} = 4 \text{ mW}$

**p.479**, problem 10.16: Use  $0.05 \text{ m/s} < V_a < 5 \text{ m/s}$

**p. 480**, problem 10.19: All the temperatures should be in Kelvin.

**p. 480**, problems 10.20 and 10.21: Use  $h_{fg} = 2.3 \times 10^6 \frac{\text{J}}{\text{kg}}$  and  $\sigma = 0.060 \text{ N/m}$ .

#### Chapter 11: Mass Transfer in Fluids

**p. 521**, problem 11.3:  $Le = 1$

#### Chapter 12: Radiation Heat Transfer

**p. 529**, The beginning of the first full paragraph should read "Setting  $dE_\lambda/d\lambda = 0 \dots$ "

**p. 569**, problem 12.3: Instead of reading that the plate "is insulated on the backside," the problem statement should read that the plate is "heated on the backside."

p. 571, problem 12.15: Use Figure 12.27 for this problem.

p. 572, problem 12.17:

- $T_H = 600 \text{ K}$
- "Panel" should be replaced with "plate."
- The variable " $w_s$ " should be replaced with " $w_H$ ."

p. 573, problem 12.19: The tabulated view factor,  $F_{21}$ , is  $F_{21} = \frac{1}{2} \left\{ 1 - \left[ 1 + \left( \frac{D}{L} \right)^2 \right]^{-1/2} \right\}$

Appendix II: Equations of motion and thermal energy balance

p. 579: The next to last terms in the three Navier-Stokes equations in Cartesian coordinates should be  $\frac{\partial}{\partial y} \left( \frac{\partial u}{\partial y} \right)$ ,  $\frac{\partial}{\partial y} \left( \frac{\partial v}{\partial y} \right)$ , and  $\frac{\partial}{\partial y} \left( \frac{\partial w}{\partial y} \right)$ .